



## RuO<sub>2</sub>–SnO<sub>2</sub> nanocomposite electrodes for methanol electrooxidation

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### ABSTRACT

The RuO<sub>2</sub>–SnO<sub>2</sub> nanostructured electrodes for methanol electrooxidation are prepared by means of colloidal synthetic method. Using X-ray diffraction method and transmission electron microscopy, it is observed that the crystallinity of nanocomposite supports is increased with heat treatment due to an increased crystallinity of SnO<sub>2</sub> and RuO<sub>2</sub> nanophases with ~5 nm in size. In the case of the RuSnO<sub>2</sub> supported catalysts, Pt nanocatalysts with ~3 nm in size are well dispersed and mixed with RuSnO<sub>2</sub> nanocomposite supports. Using an electrochemical and thermogravimetric analysis, it is found that the RuSnO<sub>2</sub> supported catalysts show an excellent catalytic activity and stability in comparison with Vulcan XC-72 supported catalyst. Furthermore, compared to the Pt catalyst supported by as-prepared RuSnO<sub>2</sub>, the Pt catalyst supported by RuSnO<sub>2</sub> heated at 400 °C displays an excellent catalytic activity and stability, which could be due to an increased crystallinity caused by heat treatment.

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### 1. Introduction

Direct methanol fuel cells (DMFCs) have attracted considerable interest because of a variety of merits such as low operating temperatures, ease of handling a liquid fuel, the high energy density of methanol, and applications to micro-sized fuel cells [1,2]. The excellent catalytic activity of platinum for methanol oxidation, especially, at low temperatures makes this metal electrocatalyst ideal for use as an anode in DMFCs. However, to confirm an excellent performance and stability of the fuel cell, such an electrode consists of a metallic nanophase and a porous material as a support for the nanoparticles.

Typically, carbon-based nanomaterials have been used as promising supports for low temperature fuel cells. Carbon black has been well known as an ideal material for supporting nanosized metallic particles in the electrode for polymer electrolyte membrane fuel cells. However, kinetically slow, yet thermodynamically favourable electrochemical oxidation of carbon at fuel cell potentials limits long-term stability of the supported catalysts [3–14]. Despite the relatively low operation temperature in the fuel cell, the electrode encounters conditions favourable to oxidation such as the presence of oxygen, liquid water, and high potentials. Accordingly, carbon substitutes are extremely needed for much longer life time in fuel cell operation.

In general, the requirements of support materials for their applications to the supports for platinum-based electrocatalyst

are a high surface area for well-dispersion of nanosized catalysts, low electrical resistance to facilitate electron transport during the electrochemical reactions, a pore structure suitable for maximum contact with fuel or oxidant and strong interaction between the catalyst and the support. Especially, oxide supports have been widely used in heterogeneous catalysis and have inherently higher stability than carbon in oxidizing environments. Among them, tin oxides have been attractive as supports due to stability in fuel cell operation atmosphere, low cost, commercial availability, and stability in water. The stoichiometric SnO<sub>2</sub> is a semiconductor with a band gap of 3.0–3.2 eV at room temperature [15–19]. However,

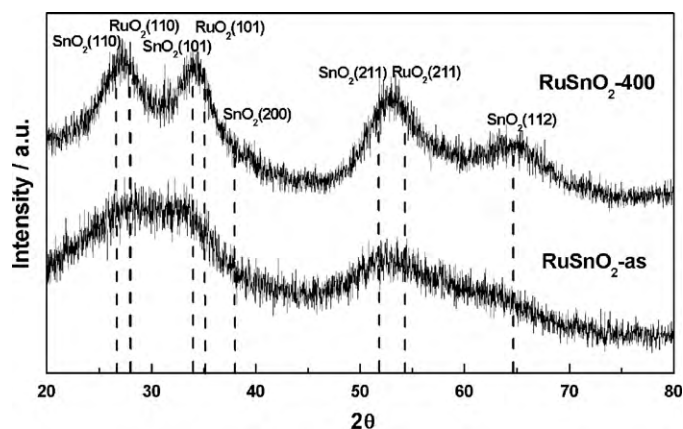


Fig. 1. XRD patterns for as-synthesized RuO<sub>2</sub>–SnO<sub>2</sub> (RuSnO<sub>2</sub>-as) and RuO<sub>2</sub>–SnO<sub>2</sub> annealed at 400 °C (RuSnO<sub>2</sub>-400).

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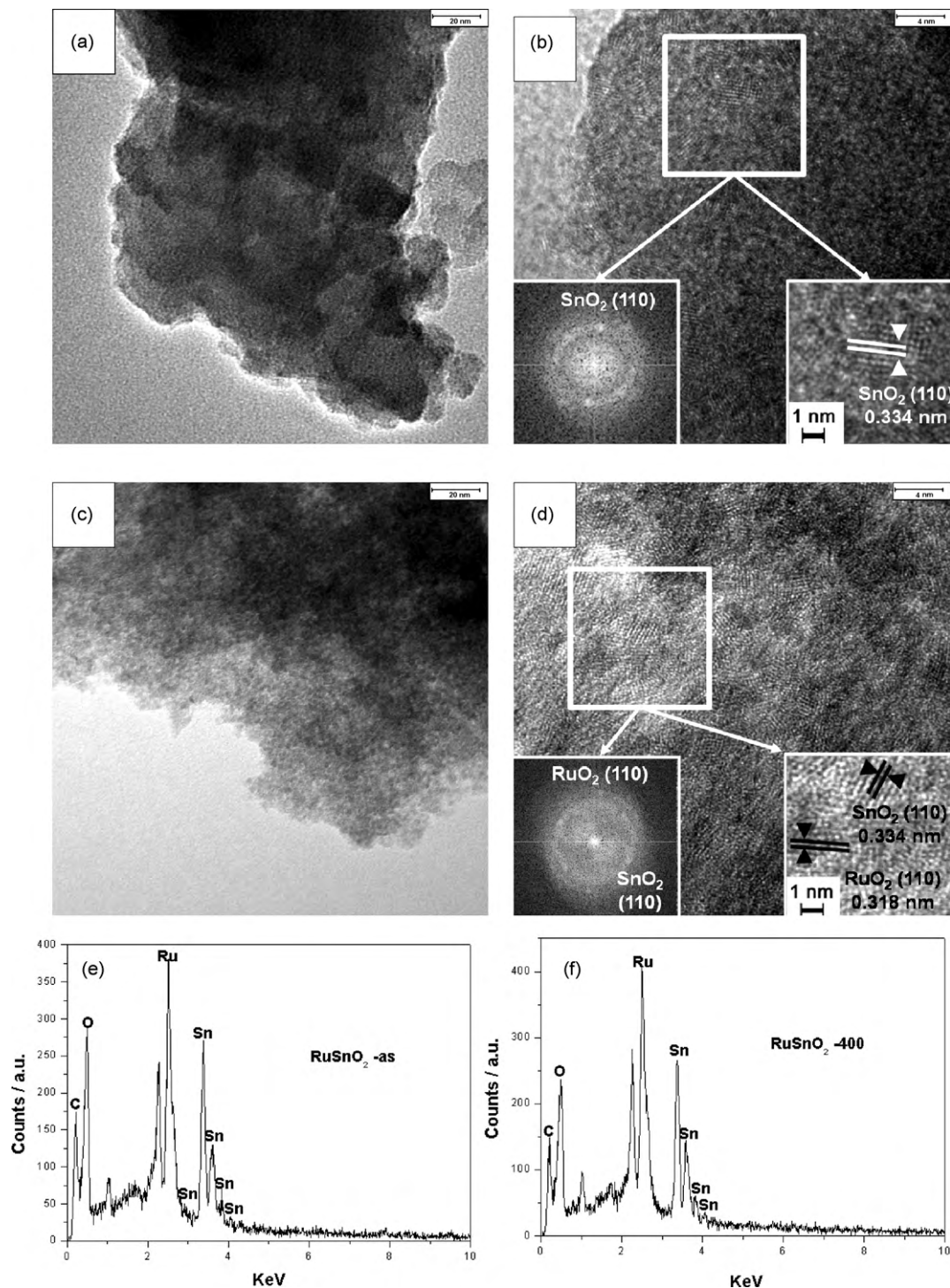
for electrochemical applications such as DMFC, an excellent electronic conductivity of  $\text{SnO}_2$  is necessarily required. The methods to improve an electronic conductivity of  $\text{SnO}_2$  are reduction of pure tin oxide by introducing appropriate dopants (F or Sb) and conducting materials (polymer or oxide) in the oxide [20–24].

In this paper, we prepared  $\text{RuO}_2\text{-SnO}_2$  nanocomposite electrode as a support for DMFCs and evaluated electrochemical properties of  $\text{RuO}_2\text{-SnO}_2$  supported Pt catalysts compared to those of conventional carbon supported Pt catalyst. The structural and electrochemical properties of the supported catalysts were char-

acterized using transmission electron microscopy (TEM), energy dispersive X-ray spectroscopy (EDX) X-ray diffraction (XRD), voltammetry, and thermogravimetric analysis (TGA).

## 2. Materials and methods

The  $\text{RuO}_2\text{-SnO}_2$  nanocomposite electrode with an atomic ratio of Sn:Ru = 50:50 was prepared by colloidal synthetic method [25].  $\text{SnCl}_4\cdot 5\text{H}_2\text{O}$  and  $\text{RuCl}_3\cdot 3\text{H}_2\text{O}$  were used as precursors. The  $\text{SnCl}_4\cdot 5\text{H}_2\text{O}$  (1.13 g, Aldrich) and  $\text{RuCl}_3\cdot 3\text{H}_2\text{O}$  (0.916 g, Aldrich) were completely dissolved in de-ionized water at 25 °C, and then  $\text{NaHSO}_3$  (4 g, Aldrich) was added to the precursor solution with continuous stirring for 1 h.



**Fig. 2.** FE-TEM images and energy dispersive X-ray spectrum of  $\text{RuSnO}_2\text{-as}$  (a, b and e) and  $\text{RuSnO}_2\text{-400}$  (c, d and f). The insets of Fig. 2(b) and (d) are selection area diffraction patterns (bottom right) and high-resolution TEM images (bottom left) of the samples, respectively.

For the prevention of reverse reaction, the pH value of the mixture was adjusted by 0.6 M  $\text{Na}_2\text{CO}_3$  (Aldrich) solution to 5. Then hydrogen peroxide (5 mL) was added to the mixture solution with a flow rate of  $1 \text{ mL min}^{-1}$ . The pH of the solution must be adjusted to 5 for prevention of reverse reaction. After stirring at room temperature for 1 h, the precipitated powders were repeatedly washed and filtrated with distilled de-ionized water until impurities were completely removed. The powders were dried at  $80^\circ\text{C}$  oven for 6 h. The resulting powder was heated at  $400^\circ\text{C}$  for 2 h in air atmosphere.

To prepare  $\text{RuO}_2\text{-SnO}_2$  supported Pt (40 wt%) catalysts, the  $\text{RuO}_2\text{-SnO}_2$  powders (0.1 g) were dispersed into de-ionized water and then  $\text{H}_2\text{PtCl}_6 \cdot 6\text{H}_2\text{O}$  (Aldrich) was added to the solution and mixed for 1 h. After 1 h,  $\text{NaBH}_4$  (Aldrich) solution as a reductant with an excess amount was added to the mixture solution with continuous stirring at  $25^\circ\text{C}$  for 2 h. The resulting precipitate was washed with de-ionized water and then was dried at  $80^\circ\text{C}$  oven.

The supports and catalysts were characterized by transmission electron microscopy (TEM) using a Philips CM20T/STEM Electron Microscope system at 200 kV. TEM samples were prepared by placing a drop of the catalyst suspension with ethanol on a carbon-coated copper grid. The elemental composition of the catalysts was investigated by energy dispersive X-ray spectroscopy (EDX, JEOL). Structural analysis of the catalysts was carried out using a Rigaku diffractometer equipped with a  $\text{Cu K}\alpha$  radiation source of  $\lambda = 0.15418 \text{ nm}$  with a Ni filter. The tube current was 100 mA with a tube voltage of 40 kV. The  $2\theta$  between  $20^\circ$  and  $80^\circ$  were explored at a scan rate of  $4^\circ \text{ min}^{-1}$ . Thermogravimetric analysis (TGA) curves were obtained in a thermal analyzer (SDT Q-600, TA Instruments) in the range of  $30\text{--}800^\circ\text{C}$  at a heating rate of  $10^\circ\text{C min}^{-1}$  in air flow of  $60 \text{ cm}^3 \text{ min}^{-1}$ .

Electrochemical measurements were carried out using a three electrode cell. A Pt gauze and  $\text{Ag}/\text{AgCl}$  (in saturated KCl) were used as a counter and reference electrode, respectively. The glassy carbon electrode as a working electrode was polished with 1, 0.3, and  $0.05 \mu\text{m}$   $\text{Al}_2\text{O}_3$  paste and then washed in de-ionized water. The catalyst ink was prepared by ultrasonically dispersing catalyst powders in an appropriate amount of Millipore water. The electrode was coated onto a glassy carbon working electrode with  $4 \mu\text{L}$  of the catalyst ink. After drying at  $50^\circ\text{C}$  oven, the total loading of catalyst was  $50 \mu\text{g cm}^{-2}$ . The solutions of  $0.5 \text{ M H}_2\text{SO}_4$  and  $2 \text{ M CH}_3\text{OH} + 0.5 \text{ M H}_2\text{SO}_4$  were continuously stirred and purged with nitrogen. To identify electrochemical properties and catalytic activity of the catalysts, cyclic voltammograms (CVs) for the catalysts were obtained using a potentiostat (Eco Chemie, AUTOLAB) at room temperature with a scan rate of  $50 \text{ mV s}^{-1}$ . The current versus time curve for methanol electrooxidation of the catalysts was measured at  $0.4 \text{ V}$  for 600 s. All potentials are reported with respect to  $\text{Ag}/\text{AgCl}$ .

### 3. Results and discussion

Fig. 1 shows XRD patterns for as-prepared  $\text{RuO}_2\text{-SnO}_2$  ( $\text{RuSnO}_2\text{-as}$ ) and  $\text{RuO}_2\text{-SnO}_2$  heat treated at  $400^\circ\text{C}$  ( $\text{RuSnO}_2\text{-400}$ ). To investigate the structure of Sn and Ru oxide phases, as shown in Fig. 1, the XRD patterns of  $\text{RuO}_2\text{-SnO}_2$  were obtained representing the characteristic peaks of typical  $\text{SnO}_2$  structure, that is, (1 1 0) at  $2\theta = 26.6^\circ$ , (1 0 1) at  $2\theta = 33.8^\circ$ , (2 0 0) at  $2\theta = 37.9^\circ$ , (2 1 1) at  $2\theta = 51.7^\circ$ , and (1 1 2) at  $2\theta = 64.7^\circ$ . The XRD patterns from the peaks in the  $\text{RuSnO}_2\text{-as}$  seem to be mainly associated with tetragonal  $\text{SnO}_2$ , whereas there seem to be no diffraction peaks of Ru oxides because of an amorphous phase. However, since it is hard to distinguish crystal phases just simply based on the XRD patterns, TEM analysis for the  $\text{RuSnO}_2$  will be described (Fig. 2). The presence of ruthenium oxide in the  $\text{RuSnO}_2\text{-400}$  is clearly revealed by characteristic diffraction peaks of (1 1 0), (1 0 1), and (2 1 1) planes at  $2\theta = 28^\circ$ ,  $35^\circ$ , and  $54.2^\circ$ , respectively. It is expected that the degree of crystallization increases with heat treatment due to transition of amorphous to crystalline phase, which means that the heat treatment could improve crystallinity of  $\text{SnO}_2$  and  $\text{RuO}_2$ .

The nanostructures of  $\text{RuSnO}_2\text{-as}$  and  $\text{RuSnO}_2\text{-400}$  are shown in Fig. 2. The  $\text{RuSnO}_2\text{-as}$  displays relatively uniform nanostructures with average crystallite size of  $\sim 4 \text{ nm}$ , as shown in Fig. 2(a). However, crystalline phases with clear lattice fringes are appeared in the  $\text{RuSnO}_2\text{-as}$  (Fig. 2(b)), which the spacing of  $0.334 \text{ nm}$  in crystalline phases corresponds to the (1 1 0) plane of  $\text{SnO}_2$ . In contrast, the  $\text{RuSnO}_2\text{-400}$  consists of crystalline structure with average crystallite size of  $\sim 5 \text{ nm}$ , as shown in Fig. 2(c). In the TEM image of the  $\text{RuSnO}_2\text{-400}$ , the d-spacings of  $0.334$  and  $0.318 \text{ nm}$  are attributed to the (1 1 0) planes of  $\text{SnO}_2$  and  $\text{RuO}_2$  (Fig. 2(d)). Accordingly, it is evident that from the TEM analysis, the  $\text{RuSnO}_2\text{-as}$  and  $\text{RuSnO}_2\text{-400}$  suggest nanocomposite supports consisting of  $\text{RuO}_2$  and  $\text{SnO}_2$ .

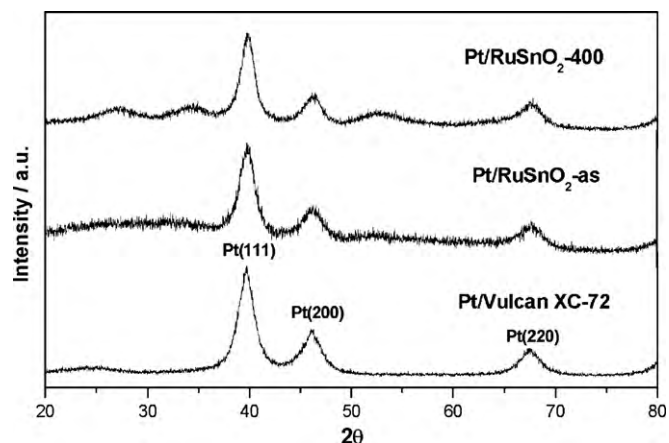
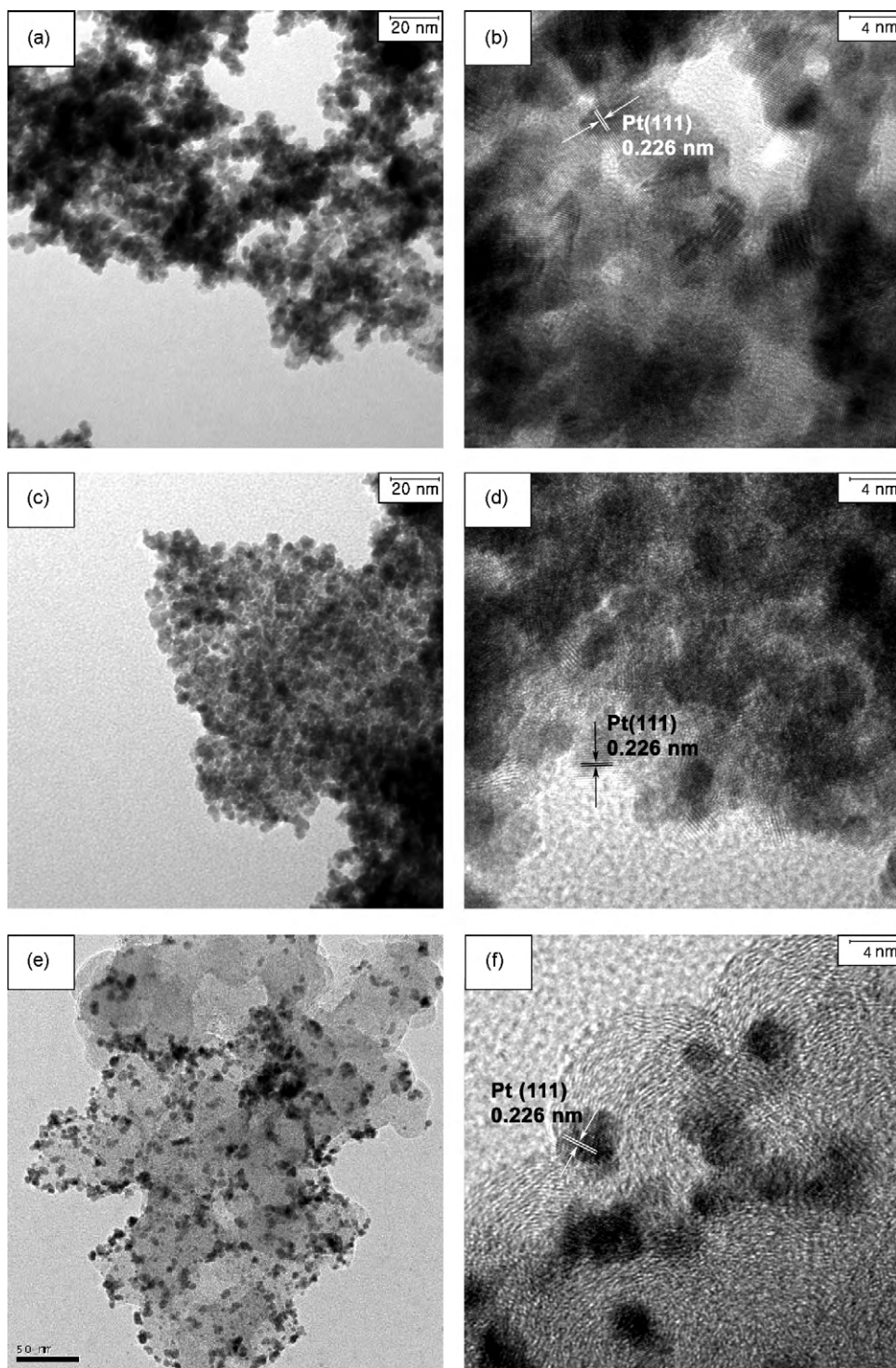


Fig. 3. XRD patterns of  $\text{Pt}/\text{RuSnO}_2\text{-as}$ ,  $\text{Pt}/\text{RuSnO}_2\text{-400}$ , and  $\text{Pt}/\text{Vulcan XC-72}$ .

The elemental compositions of the nanocomposite electrodes were investigated using an EDX analysis as shown in Fig. 2(e) and (f). The atomic ratio of Ru: Sn in the supports is the nominal composition, which is in good agreement with the intentional one.

Fig. 3 shows XRD patterns of  $\text{RuSnO}_2\text{-as}$  and  $\text{RuSnO}_2\text{-400}$  supported Pt (Pt 40 wt%) catalysts ( $\text{Pt}/\text{RuSnO}_2\text{-as}$  and  $\text{Pt}/\text{RuSnO}_2\text{-400}$ , respectively) compared to that of Vulcan XC-72 supported Pt catalyst ( $\text{Pt}/\text{Vulcan XC-72}$ ). The presence of platinum crystalline structures is clearly revealed by the characteristic diffraction peaks at  $2\theta = 39.7^\circ$ ,  $46.2^\circ$  and  $67.4^\circ$ , which are associated with (1 1 1), (2 0 0) and (2 2 0) planes, respectively. All the XRD patterns clearly show the characteristic peaks of face-centered-cubic structure of Pt crystalline. Fig. 4 shows FE-TEM images of the supported Pt catalysts. The Pt nanoparticles with average crystallite size of  $\sim 3 \text{ nm}$  are well dispersed and mixed with  $\text{RuSnO}_2\text{-as}$  and  $\text{RuSnO}_2\text{-400}$  nanocomposite supports. In the  $\text{Pt}/\text{RuSnO}_2\text{-as}$  (Fig. 4(a) and (b)) and  $\text{Pt}/\text{RuSnO}_2\text{-400}$  (Fig. 4(c) and (d)), the presence of Pt nanoparticles is clearly revealed by lattice fringes with (1 1 1) d-spacing of  $0.226 \text{ nm}$ . However, the  $\text{RuSnO}_2\text{-as}$  consists of crystalline  $\text{SnO}_2$  and amorphous  $\text{RuO}_2$  while the  $\text{RuSnO}_2\text{-400}$  shows both crystalline  $\text{SnO}_2$  and  $\text{RuO}_2$ . Accordingly, the  $\text{RuSnO}_2$  supported Pt catalysts are nanocomposite structure consisting of Pt nanocatalysts and  $\text{SnO}_2\text{-RuO}_2$  nano-supports while Pt catalysts in the  $\text{Pt}/\text{Vulcan XC-72}$  (Fig. 4(e) and (f)) are deposited on carbon supports ( $20\text{--}50 \text{ nm}$  in size).

Fig. 5 shows typical cyclic voltammograms (CVs) of  $\text{RuSnO}_2$  supported Pt catalysts in  $0.5 \text{ M H}_2\text{SO}_4$  compared with  $\text{Pt}/\text{Vulcan XC-72}$ . The electrochemical characteristic curves indicate adsorption and desorption region of hydrogen and oxygen as typically observed in polycrystalline platinum electrode. However, the  $\text{RuSnO}_2$  supported Pt catalysts display thick double layer in the CVs due to oxide species of Ru and Sn compared to  $\text{Pt}/\text{Vulcan XC-72}$ . To characterize catalytic activity toward methanol electrooxidation of the supported Pt catalysts, as shown in Fig. 6(a), CVs were obtained in  $2 \text{ M CH}_3\text{OH} + 0.5 \text{ M H}_2\text{SO}_4$ . The  $\text{RuSnO}_2$  supported Pt catalysts show higher oxidation current compared with  $\text{Pt}/\text{Vulcan XC-72}$ . This may be primary attributed to oxygen species of  $\text{RuO}_2$  and  $\text{SnO}_2$  and nanocomposite structure of supports. Especially, it is considered that the nanocomposite structure of  $\text{RuO}_2$  and  $\text{SnO}_2$  could enhance catalytic activity towards methanol oxidation and reduce the poisoning effect of catalysts from the intermediates [26]. Also, the  $\text{Pt}/\text{RuSnO}_2\text{-400}$  shows still higher methanol electrooxidation current than that of the  $\text{Pt}/\text{RuSnO}_2\text{-as}$ . This means that such an enhanced catalytic activity of the  $\text{Pt}/\text{RuSnO}_2\text{-400}$  is attributed to an increased crystallinity of oxide support by means of heat treatment. As shown in Fig. 6(b), chronoamperometry (CA) for the  $\text{RuSnO}_2$  supported Pt catalysts was measured at  $0.4 \text{ V}$  in



**Fig. 4.** FE-TEM images of Pt/RuSnO<sub>2</sub>-as (a and b), Pt/RuSnO<sub>2</sub>-400 (c and d), and Pt/Vulcan XC-72 (e and f).

2 M CH<sub>3</sub>OH + 0.5 M H<sub>2</sub>SO<sub>4</sub> compared with Pt/Vulcan XC-72. The sequence of catalytic activity for methanol electrooxidation is as follows: Pt/RuSnO<sub>2</sub>-400 > Pt/RuSnO<sub>2</sub>-as > Pt/Vulcan XC-72. The enhanced catalytic activity and stability of the Pt/RuSnO<sub>2</sub>-400 are due to an increased crystallinity in the nanocomposite support in comparison with the Pt/RuSnO<sub>2</sub>-as, which might result from improved electrical conductivity of the support as follows: electrical conductivity values of RuSnO<sub>2</sub>-as and RuSnO<sub>2</sub>-400 are  $6.7 \times 10^{-5}$  and  $3.8 \times 10^{-2} \text{ S cm}^{-1}$ , respectively.

**Fig. 7** shows thermogravimetric analysis (TGA) curves of supported catalysts in the range of 30–800 °C in air flow. The normalized weight loss of Pt/Vulcan XC-72 is ~80%, which is dominantly attributed to oxidation of the carbon support at around 400 °C. On the other hand, the RuSnO<sub>2</sub> supported Pt catalysts show extremely slight weight loss of ~3%, which means an excellent stability of the RuSnO<sub>2</sub> supports. Thus, the electrochemical stability of the RuSnO<sub>2</sub> supported Pt catalysts could be attributed to corrosion resistance of RuSnO<sub>2</sub> compared to Vulcan XC-72.

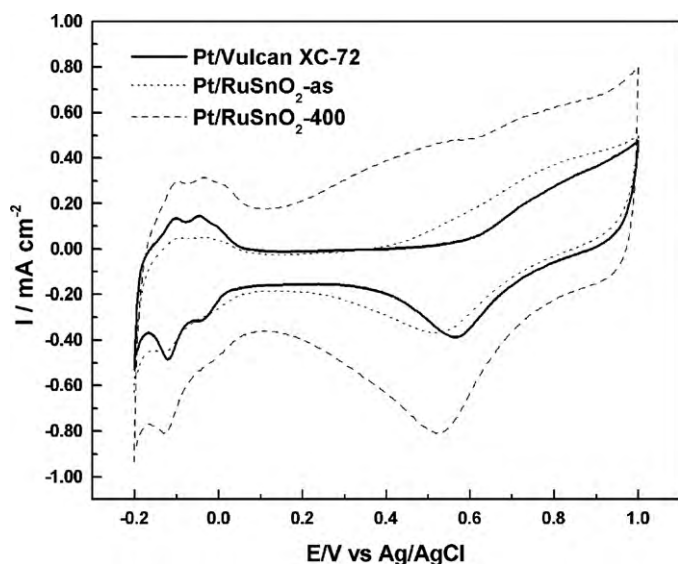


Fig. 5. CVs of supported Pt catalysts in 0.5 M  $\text{H}_2\text{SO}_4$  with a scan rate of  $50 \text{ mV s}^{-1}$  at  $25^\circ\text{C}$ .

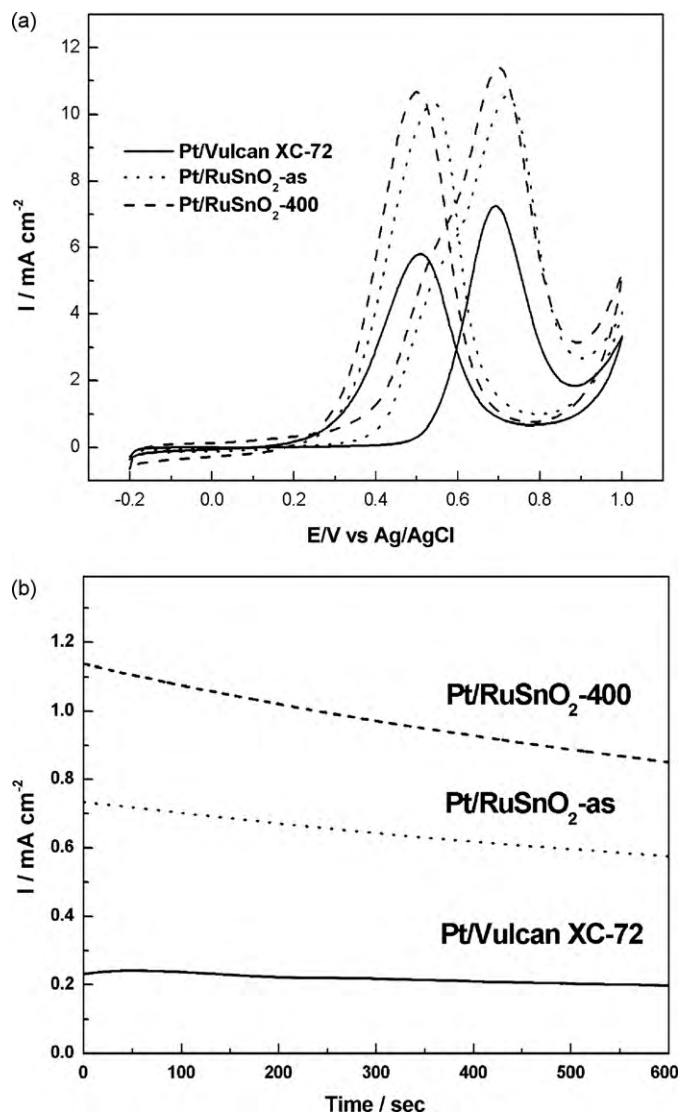


Fig. 6. (a) CVs and (b) plots of oxidation current versus time for supported Pt catalysts in  $2 \text{ M CH}_3\text{OH} + 0.5 \text{ M H}_2\text{SO}_4$  at  $25^\circ\text{C}$ .

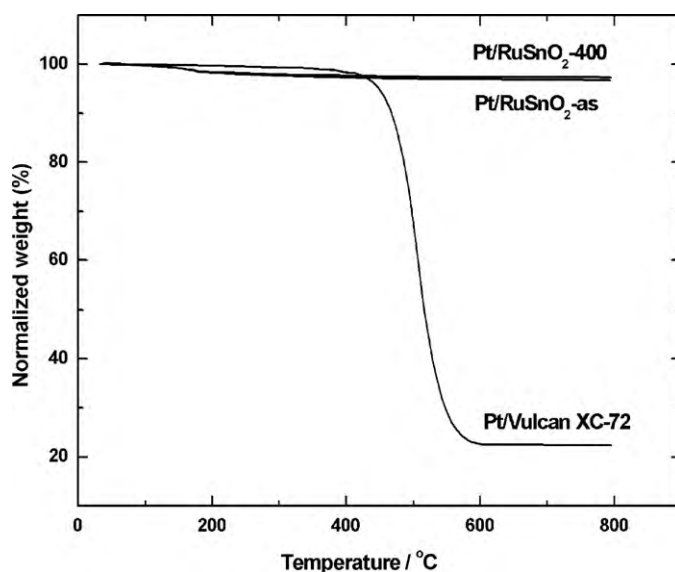


Fig. 7. TGA curves of supported catalysts in the range of  $30\text{--}800^\circ\text{C}$  with a heating rate of  $10^\circ\text{C min}^{-1}$  in air flow of 60 SCCM.

#### 4. Conclusions

The  $\text{RuO}_2\text{-SnO}_2$  nanocomposite supported catalysts for methanol electrooxidation were synthesized. In the case of the  $\text{RuSnO}_2$  supported catalysts, Pt nanocatalysts with average crystallite size of  $\sim 3 \text{ nm}$  were well dispersed and mixed with  $\text{RuSnO}_2$  nanocomposite supports with 4–5 nm in size. The  $\text{RuSnO}_2$  supported Pt catalysts showed higher oxidation current in comparison with Pt/Vulcan XC-72. Furthermore, the methanol electrooxidation current of the  $\text{RuSnO}_2\text{-400}$  supported Pt catalyst was higher than that of the  $\text{RuSnO}_2\text{-as}$  supported Pt catalyst. The improved catalytic activity and catalytic stability of the  $\text{RuSnO}_2\text{-400}$  supported Pt catalyst could be attributed to increased crystallinity and electrical conductivity of oxide support caused by heat treatment and corrosion resistance of  $\text{RuSnO}_2$ .

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